The results shown in Table 2 demonstrate that the catalysts of the invention exhibit very high NO₂ decomposition performance even at temperatures below 300°C. On the other hand, with Comparative Example 1 which had Pt and Ba both present on the γ -alumina carrier, the NO₂ decomposition performance was slightly lower than that of the catalysts of the invention. The catalyst of Comparative Example 2 exhibited absolutely no NO2 decomposition performance. The reason is believed to be its structure wherein no catalyst was carried on the filter.

Page 12, table 3, delete current table and insert therefor:

Table 3 Comparison of particulate matter (PM) combustion rates

| B" | | Catalyst | | PM combustion rate (mg/sec/L) | |
|----|--------------------------|--|--|-------------------------------|---------------|
| | | NO oxidation catalyst | NO ₂ decomposition catalyst | 200°C | 250°C |
| | Example 1 Example 2 | Pt/WO ₃ /ZrO ₂ Pt/WO ₃ /ZrO ₂ | Pt/Ba/γ-alumina Fe/γ-alumina | 0.04 0.04 | 0.12 0.11 |
| | Comp. Ex.1 Comp. Ex.2 | Pt/Ba/γ-alumina Upstream Pt/silica + monolith filter | | 0.012 0.002 | 0.05 0.006 |

Catalyst components: (2 g Pt + 0.1 g Rh)/1L filter

IN THE CLAIMS:

Please add new claims 7-10 as follows:

- A particulate matter combustion catalyst according to claim 1, wherein said --7. NO oxidation catalyst and NO₂ decomposition catalyst are carried on a particulate matter filter.--
- --8. A particulate matter combustion catalyst according to claim 2, wherein said NO oxidation catalyst and NO₂ decomposition catalyst are carried on a particulate matter filter.--

